

Sanborn, Head & Associates, Inc. 1 Technology Park Drive Westford, MA 01886 978-392-0900

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SANBORN, HEAD & ASSOCIATES, INC.

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Tom Sudol Project Manager

(IF ENCLOSURES ARE NOT AS NOTED, PLEASE NOTIFY US IMMEDIATELY)

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Memorandum

To:	Bill	Clark	Liberty	Utilities
~ ~ ·				

From: Joan Fontaine and Mike Nicoloro

File: 3672.00

Date: August 31, 2015

Re: LNG Facility Fatal Flaw Siting Analysis for West Lebanon, NH Parcel – Initial Phase

cc: Tom Sudol, Maxwell Quinn | Sanborn Head

<u>Project Overview</u>

Liberty Utilities is evaluating a parcel of land in West Lebanon, NH for the potential siting of an LNG storage and vaporization facility. Liberty Utilities requested Sanborn Head to perform an analysis to assess if there are any fatal flaws with respect to siting an LNG facility. The proposed LNG facility is anticipated to have

natural gas sendout piping. It is also anticipated that CNG tube trailers will deliver CNG to the facility for use in up to six decompression skids.

Tasks Performed As Part of Initial Phase of Analysis

1. Preliminary Design Basis

We prepared a preliminary design basis that addresses LNG flow rates and natural gas send out flow rates (peak hourly) and associated fluid temperatures and pressures, as well as number of days of on-site storage. A summary table is provided as an attachment to this memo. Key points of the design basis are:

- a. The maximum hourly sendout from the proposed LNG facility is 358 MSCFH which is based on a peak demand estimate from Liberty Utilities.
- b. The on-site LNG storage provides an estimated four days of storage for uninterruptible users.
- c. It is assumed that the MAOP of the distribution system will be 60 psig and upstream pressure requirements were estimated based on this MAOP.
- 2. Data Review Publicly Available and Phase 1 Environmental Site Assessment Report (ESA)

We reviewed publicly available information to assess the proximity of the property to an airport and flood plains. Liberty Utilities also provided a Phase 1 ESA performed for the property for another entity. The findings from this data review

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are outlined below. Additionally, Sanborn Head has extensive knowledge of the property to the north of the parcel being evaluated – the Lebanon Landfill. Our knowledge of this property as it may relate to the parcel south of it is provided below as well.

- a. The Lebanon Municipal Airport's runway is located approximately 6,750 feet (1.3 miles) to the east of the property. This distance does not pose any issue for the layout of the proposed LNG facility with respect to runway and approach distances. Reference Drawing G-1, Location Plan, which depicts where the property is with respect to the airport.
- b. Review of both the ESA and the Federal Emergency Management Agency's National Flood Insurance Program published mapping indicate that there are not any flood plains on the property. Refer to Drawing G-3, Site Plan Flood Plains, which depicts where the flood plain is located with respect to the property.
- c. Geology We did hit bedrock unexpectedly during the construction of the last cell. There was an error in the bedrock map provided to us. The mapping we have doesn't include the property to the south, so we cannot comment offered on the depth to bedrock. However, considering the information we have to the north, the change in the river direction, bedrock could have a localized high point almost anywhere. That said, considering that the site is a sand and gravel operations, there should be drilling logs that may provide information about bedrock. Also, if continued excavation is a concern, perhaps the site development could involve engineered backfill areas. In this case the backfilling operations should be monitored to assure that a well-compacted foundation is constructed.
- d. Landfill Gas Prior to the installation and operation of the active LFG extraction system, there were some LFG migration issues detected along the landfill's east property boundary. The active system should be the mitigation for this condition. LFG migration to the south is less likely because of the unlined landfill is quite a distance away from the south boundary and the newest landfill cell is significantly deeper than the bottom of the older cells (lined and unlined). Of note is that there are plans (not yet permitted) to expand the landfill further south. This phase of the landfill is some years off. While it is not impossible for LFG to migrate from the unlined cell, or even the lined cell of the landfill gas conveyance piping, if things are well managed, the potential risk is limited.
- e. Wetland areas Considering the site usage, there may be wetlands on the site that could affect the site development. Such information is not typical of an ESA, and a wetland scientist would need to visit the site to verify the presence or absence of wetlands.

3. Conceptual Equipment General Arrangement

We prepared a conceptual equipment general arrangement drawing that depicts the major system components for the proposed LNG facility. Set back and equipment separation distances and containment requirements in accordance with NFPA 59A were incorporated into this conceptual equipment general arrangement. Reference Drawing G-4, Equipment General Arrangement, provided as an attachment to this memo.

4. Site Plan Drawing

Refer to Drawing G-2, Site Plan, which overlays the equipment general arrangement onto the property. At this preliminary phase, we did not include the proposed CNG equipment or truck egress and access routes.

5. Conceptual Level Thermal Radiation Modeling

We performed conceptual level thermal radiation modeling using LNGFire3 modeling software. Climactic data from the last six years was researched to establish the input parameters to the model (e.g., wind speed, relative humidity, temperature) in accordance with the regulations. Exclusion zone radii are depicted on the site plan developed in Item 4, above. Code requires that the 10,000 BTU/hr-ft² zone stay within the property boundaries; this is achievable based on this first round of modeling. The modeling printout is provided as an attachment.

Conclusions

The first phase of this fatal flaw analysis has not identified any fatal flaws in areas studied that would pre-empt Liberty Utilities from proceeding with the next level assessment.

Recommended Next Steps

Performing vapor dispersion modeling will be a critical aspect to more definitively qualify the property being considered. We strongly recommend that the vapor dispersion modeling be performed as soon as possible, since it is our experience that keeping the 50% LEL exclusion zone within the property boundaries is typically more challenging than keeping the 10,000 BTU/hr-ft² exclusion zone within the property boundaries. Please note that the recommended vapor dispersion modeling will provide worse case conditions. It may even show that the 50% LEL will travel beyond the property limits. Mitigation measures such as insulated concrete, vapor fences and water spray systems would be studied in the detailed design phase if we conclude that the 50% LEL goes beyond property boundaries.

As part of this next phase of the analysis, we may need to consider reducing the amount of on-site storage, using smaller LNG tanks, and optimizing the size of the subimpoundment within the LNG containment in order to meet exclusion zone requirements. Each of these elements will have an impact on the extent of the modeled vapor dispersion zones.

JMF/MAN: jmf

Encl. Preliminary Design Basis Drawing G-1, Location Plan

Drawing G-2, Site Plan Drawing G-3, Site Plan - Flood Plains Drawing G-4, Equipment General Arrangement LNGFire3 Modeling Output

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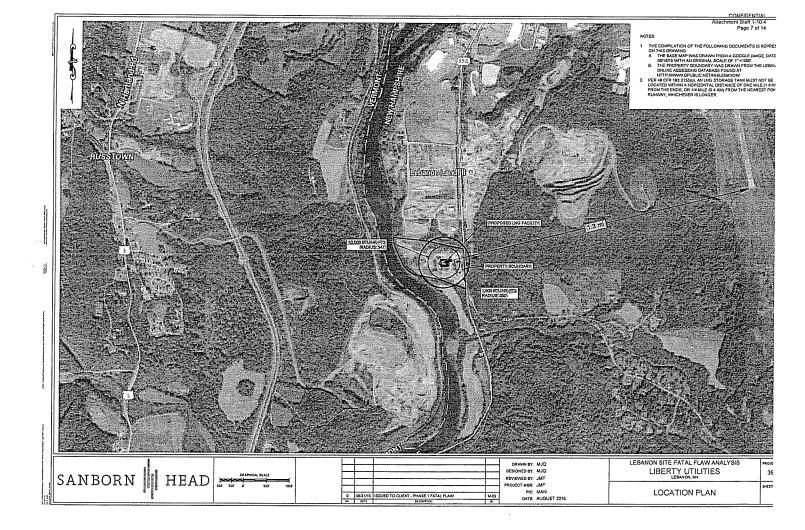
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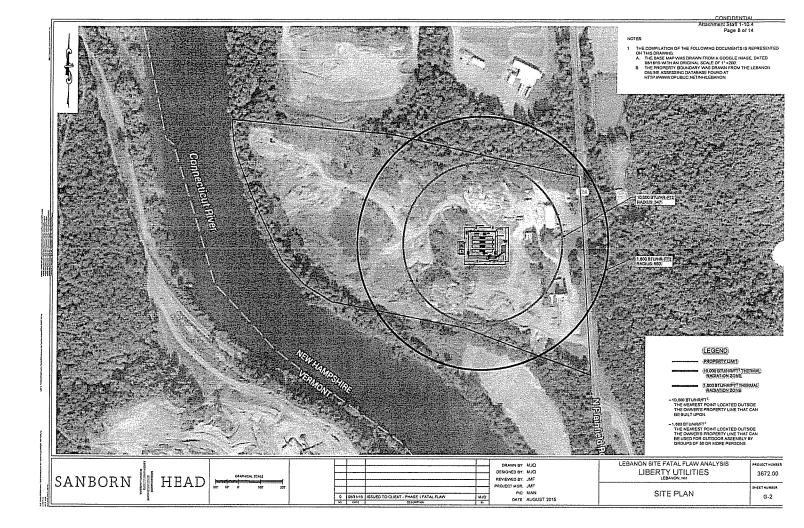
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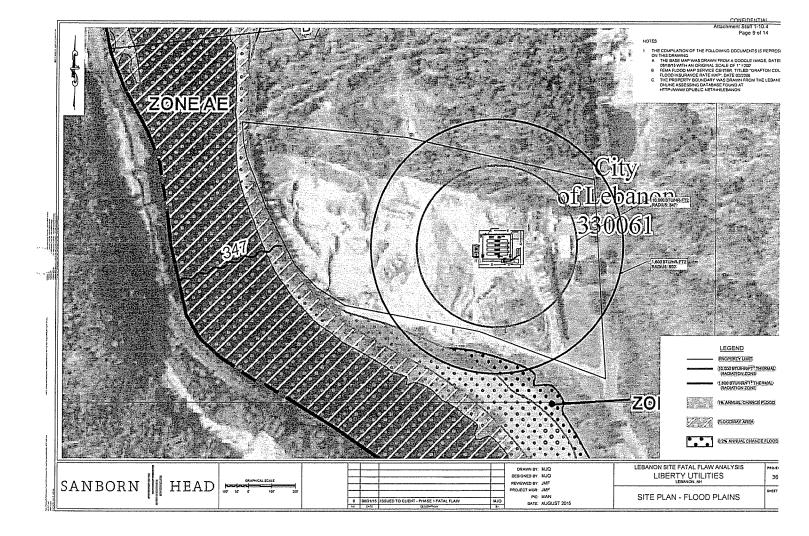
		Liberty I	Design Basis Jtilities - Lebanon NH Site	Fatal Flaw Ana	lysis
Equipment/Service	Fluid	Flow Rate	Pressure	Temperature	Comment
LNG Offloading	LNG	200 gpm (maximum)	80 psig (nominal) 100 psig (maximum)	-260 °F	(2) 100% capacity pumps, off-loading stations. Pumps to increase pressure from 20-40 psig in transports to 80 psig nominal pressure in tanks.
LNG Tanks	LNG		80 psig (nominal) 100 psig (maximum allowable)	-260 °F	
Vaporized LNG	Natural Gas	358 MSCFH (maximum) 45 MSCFH (minimum)	70 psig	50 °F	Maximum hourly flow rate based on peak demand estimate from Liberty Utilities (does not include Dartmouth College). Minimum flo rate assumes an 8:1 turndown.
NG Sendout	Natural Gas	358 MSCFH (maximum) 45 MSCFH (minimum)	60 psig	50 °F	Pressure based on distribution system MAOP.
LNG Vaporizer	TBD				6.5 MMBtu/hr - required heat output.
Boil Off Gas	Natural Gas	0.74 MSCFH	80 psig	-240 °F	Assumes a boil off rate of 0.1 % per day of the 90% full tank volume.
Boll Off Gas fter ambient heat exchanger)	Natural Gas	0.74 MSCFH	70 psig	Ambient Temperature less 20 °F	Downstream of ambient heat exchanger.

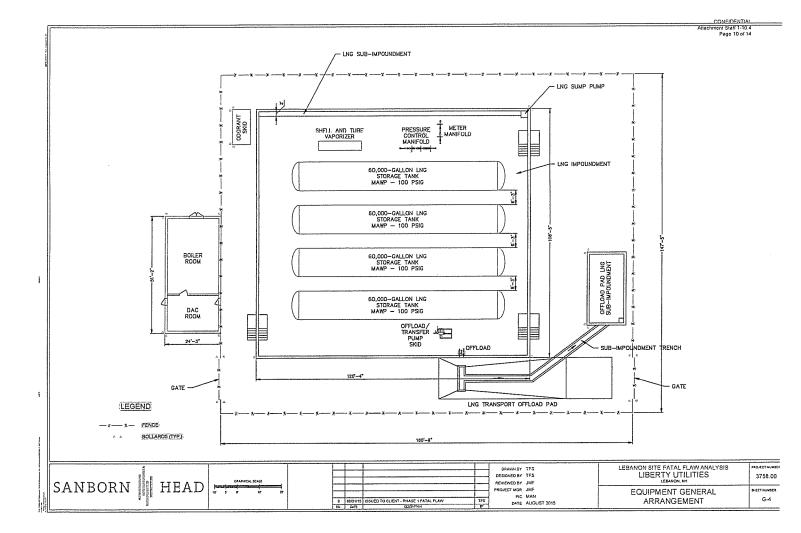
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8/12/2015









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RECTANGULAR DIKE FIRE TRENCH FIRE FUEL Name : LNG LIGHT (METHANE) Pool temperature : -258.79 ° F CONSTANT PROPERTIES Molecular weight : 16.04 Boiling point : -258.79 ° F Critical temperature : -116.68 ° F Critical pressure : 667.2 psi Heat of combustion : 2.15E+04 Btu/1b Flame temperature : 1880 ° F CALCULATED PROPERTIES Liquid compressibility factor : 0.004 Liquid density : 29.69 lb/cu ft DIMENSIONS Pool width Pool length : 147.5 ft : 181.0 ft Pool liquid height Height of flame base : 4.0 ft : 4.0 ft Height for Radiation Calculations : 4.0 ft LOCAL AMBIENT CONDITIONS Air temperature : 3.0 º F Ambient pressure : 1.0 atm Wind speed : 27.0 mph Relative humidity : 24.0% RESULTS Mass burning rate : 0.023 lb/ft' s Flame length : 207.57 ft Flame tilt from vertical (front view) : 60.14° Flame length Flame tilt from vertical (flont view) : 50.14° Flame tilt from vertical (side view) : 58.99° Flame drag ratio (front view) : 1.52 Flame drag ratio (side view) : 1.41 Maximum emissive power: 60,230 Btu/ft² hrEffective emissive power (front view): 60229.68 Btu/ft² hrEffective emissive power (side view): 60229.68 Btu/ft² hr Front view (view along dike/trench width) Thermal flux Distance from center of pool (Btu/ft² hr) (ft) -----1000 449.84 4000 563.40 1600 729.22 Side view (view along dike/trench length) ------Thermal flux Distance from center of pool (ff) (Btu/ft² hr) (ft) -----1000 447.06 4000 553.37 1600 706.63 Maximum emissive power : 190.0 kW/m**2 Front view (view along dike/trench width)

 Distance from Thermal flux to
 Thermal flux to
 Maximum flux

 center of pool
 horizontal target
 vertical target
 to target

 (ft)
 (Btu/ft² hr)
 (Btu/ft² hr)
 (Btu/ft² hr)

110.63Target in flameTarget in flameTarget in flame147.50Target in flameTarget in flameTarget in flame18450.92028.48253.814 28,482 184.38 50,920 46,751 53,814 50,823 221.25 27,572 40,701 32,383 13,484 4,203 23,538 17,814 9,864 3,292 295.00 39,309 22,339 368.75 442.50 4,205 675.72 10,721 590.00 3,360

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885.00	83.49	866.18	870.15 212.65	
1,475	9.80	212.43		
ide view (view al	ong dike/trench lengt	:h)		
Distance from center of pool (ft)	Thermal flux to horizontal target (Btu/ft ² hr)	Thermal flux to vertical target (Btu/ft' hr)	Maximum flux to target (Btu/ft' hr)	
135.75	Target in flame	Target in flame	-	
181.00	51,700	28,537	54,292	
226.25	46,029	27,286	50,136	
271.50	37,608	24,214	42,920	
362.00	15,879	17,458	23,598	
452.50	3,850	8,659	9,475	
543.00	1,127	4,172	4,321	
724.00	211.57	1,456	1,472	
1,086	30.99	418.92	420.03	
1,810	4.04	109.05	109.11	

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FUEL Name

DIMENSIONS

RESULTS

RECTANGULAR DIKE FIRE TRENCH FIRE : LNG LIGHT (METHANE) Pool temperature : -258.79 ° F CONSTANT PROPERTIES Molecular weight : 16.04 Boiling point : -258.79 ° F Critical temperature : -116.68 ° F Critical pressure : 667.2 psi Heat of combustion : 2.15E+04 Btu/lb Flame temperature : 1880 ° F CALCULATED PROPERTIES Liquid compressibility factor : 0.004 Liquid density : 29.69 lb/cu ft Pool width Pool length : 109.0 ft : 121.0 ft Pool liquid height : 4.0 ft Height of flame base : 4.0 ft Height for Radiation Calculations : 1.64 ft LOCAL AMBIENT CONDITIONS Air temperature : 3.0 ° F Ambient pressure : 1.0 atm Wind speed : 27.0 mph Relative humidity : 24.0음 Mass burning rate : 0.023 lb/ft² s Flame length : 168.21 ft Flame tilt from vertical (front view) : 61.75° Flame tilt from vertical (side view) : 61.2° Flame drag ratio (front view) Flame drag ratio (side view) : 1.57 : 1.51 Maximum emissive power: 60,230 Btu/ft² hrEffective emissive power (front view): 60229.67 Btu/ft² hrEffective emissive power (side view): 60229.67 Btu/ft² hr Front view (view along dike/trench width) Thermal flux Distance from center of pool (Btu/ft² hr) (ft) 1000 347.07 4000 430.45 1600 550.98 Side view (view along dike/trench length) Thermal flux Distance from center of pool (Btu/ft² hr) (ft) (Btu/ft? hr) (ft) 1000 345.92 4000 426.71 1600 542.61 -----______ Maximum emissive power

Front view (view along dike/trench width)

: 190.0 kW/m**2

Distance from	Thermal flux to	Thermal flux to	Maximum flux
center of pool	horizontal target	vertical target	to target
(ft)	(Btu/ft² hr)	(Btu/ft² hr)	(Btu/ft² hr)
81.75	Target in flame	Target in flame	Target in flame
109.00	Target in flame	Target in flame	Target in flame
136.25	51,564	25,283	53,266
163.50	47,767	26,254	50,890
218.00	35,543	22,694	40,739
272.50	18,413	18,323	25,975
327.00	6,272	11,362	12,977
436.00	916.51	3,688	3,800

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654.00	101.00	907.39	912.93
1,090	11.14	214.03	214.31
Side view (view al	ong dike/trench lengt	h)	
Distance from center of pool (ft)	Thermal flux to horizontal target (Btu/ft² hr)	Thermal flux to vertical target (Btu/ft² hr)	Maximum flux to target (Btu/ft² hr)
90.75 121.00 151.25 181.50 242.00 302.50 363.00 484.00 726.00 1,210	Target in flame Target in flame 49,806 44,097 28,203 10,763 3,142 485.64 59.60 7.02	Target in flame Target in flame 26,027 25,187 19,986 14,175 7,419 2,380 618.58 151.49	Target in flame Target in flame 52,254 47,797 34,005 17,798 8,057 2,429 621.43 151.65